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# Functionalized Polysilsesquioxane-Based Hybrid Silica Solid Amine Sorbents for the Regenerative Removal of CO<sub>2</sub> from Air

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**Supporting Information** 

**ABSTRACT:** Functionalized polysilsesquioxane-based hybrid silica materials are presented as solid amine sorbents for direct  $CO_2$  capture from air. The sorbent was synthesized from amine and vinyl functionalized alkoxysilanes by a simple, energy efficient, and cost-effective co-condensation method. The material, containing bound amine functionalities, was found to have a selective  $CO_2$  capturing capacity of 1.68 mmol/g from atmospheric air with an adsorption half time of 50 min. This material also showed a maximum adsorption capacity of 2.28 mmol/g in pure  $CO_2$  and 1.92 mmol/g in 10%  $CO_2$ . Desorption started at a temperature as low as 60 °C, and complete desorption occurred at 80 °C. The sorbent exhibited high recycling ability, and 100 cycles of adsorption/desorption were demonstrated in pure  $CO_2$  and 50 cycles in ambient air without any loss in efficiency.

**KEYWORDS:** silanes, silsesquioxanes, CO<sub>2</sub>, adsorption, desorption

# 1. INTRODUCTION

The feasibility of CO<sub>2</sub> capture from atmospheric air to control the increasing CO<sub>2</sub> levels has been under active discussion in the past decade. Many researchers<sup>1,2</sup> advocated for direct capture of CO<sub>2</sub> from air to reduce atmospheric CO<sub>2</sub> level and believed that it is closer to geoengineering than to conventional mitigation by industrial effluent gas treatment. The "Air as the renewable carbon source" thought was discussed by Olah et al.<sup>3</sup> At the same time, a suitable material to remove  $CO_2$ , regeneratively, from an ultradilute environment-like atmospheric air on a large scale is challenging and is still in its infancy. The most familiar materials include CaO<sup>4</sup> (CaOH)<sub>2</sub>,<sup>5</sup> NaOH<sup>6</sup> etc., which absorb CO<sub>2</sub> by chemisorption, and regeneration is energy intensive. Zeolites<sup>7,8</sup> and activated carbons<sup>9,10</sup> adsorb through physisorption but are less selective. Zeolites require high regeneration temperature, and their performance is adversely affected by humidity. Metal organic frameworks  $(MOFs)^{11-15}$  are making good impact, and recent developments<sup>16-18</sup> are highly promising toward CO<sub>2</sub> capture from dilute environments. Functionalized porous polymers<sup>19-21</sup> also form an important class of materials being investigated as promising candidates for CO<sub>2</sub> removal.

Amine-based solid sorbents<sup>22–26</sup> which hold  $CO_2$  by chemisorption have been extensively studied in the past several years as materials for  $CO_2$  capture. Amine species can be either immobilized by wet impregnation or grafted onto the porous substrates<sup>24–33</sup> like silica, activated carbon, and polymers for use as regenerable systems for  $CO_2$  removal. Most of the research articles published on mesoporous sorbents, especially



mesoporous silica with high surface area and optimum amine loading, show high  $CO_2$  removal efficiency<sup>28,29</sup> from pure  $CO_2$ , but CO<sub>2</sub> capture studies from atmospheric air are lacking. Polyethylenimine-based silica systems were studied for air capture by many investigators.<sup>30-33</sup>The higher CO<sub>2</sub> removal capability of amine-impregnated sorbents gets faded by the problem of loss in efficiency after successive regeneration cycles.<sup>3,28,29,34-36</sup> To overcome amine loss observed in amineimpregnated sorbents, aminosilanes are covalently grafted on to the intrachannel surface of mesoporous silica either through post-modification or by direct synthesis (co-condensation). Though several reports exist for the synthesis of amine-grafted silica for CO<sub>2</sub> capture using post-modification of silica with organosilanes, 7,37-40 only some of them were reported for direct capture of CO<sub>2</sub> from air. Triamine-grafted pore expanded mesoporous silica (TRI-PE-MCM-41) was reported by Sayari and co-workers<sup>41,42</sup> with a CO<sub>2</sub> capture capacity of 0.98 mmol/ g at low CO<sub>2</sub> concentration, and also the effect of humidity<sup>43</sup> on CO<sub>2</sub> adsorption of amine containing sorbents was studied. Subsequently, a breakthrough in this field was made by Jones and co-workers<sup>44</sup> by making HAS (hyperbranched amino silica) sorbent using in situ ring opening polymerization of aziridine. However, synthesis of mesoporous silica (SBA-15, MCM-41, etc.) is energy intensive as it requires calcination at temperature as high as 550  $^{\circ}$ C for 5–6 h.

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Direct synthesis via hydrolysis and co-condensation of organosilanes with aminosilanes in the presence of an organic template using acid or base catalyst produces amine functionalized mesoprous silica materials. However, only a few amine functionalized co-condensed silica materials were reported for  $CO_2$  adsorption studies.<sup>38,45–47</sup> Polysilsesquioxanes are relatively new to the class of amine sorbents and remain less explored for CO2 capture. Mesoporous amine bridged polysilsesquioxane was reported by Qi et al.48 and organicinorganic polyaspartimide involving polyhedral oligomeric silsesquioxane by Shanmugham et al.49 for CO2 removal application. Formation of fully condensed polyhedral oligomeric silsesquioxane by hydrolytic condensation of trifunctional organosilicon monomers was discussed by Voronkov and Lavrent'yev,<sup>50</sup> and they reported that octamers with ethyl and vinyl groups are formed in alcoholic media without the addition of a catalyst. Methods exist for preparing functionalized hybrid silica materials<sup>51</sup> and surface functionalized polysilsesquioxane hard spheres,<sup>52</sup> but these materials were not evaluated for CO<sub>2</sub> adsorption properties.

Synthesis of polysilsesquioxane-based hybrid silica materials for  $CO_2$  capture from air is reported here, and the use of such materials for this application is new to the best of our knowledge. Optimization strategy for producing these sorbents in good yield and with maximum  $CO_2$  adsorption, performance of the sorbent in different  $CO_2$  partial pressures, and recycling capability of the sorbent are explored in detail.

#### 2. EXPERIMENTAL SECTION

**2.1. Materials.** 3-Aminopropyl triethoxysilane (99%) and vinyl triethoxysilane (97%) were purchased from Sigma-Aldrich, and absolute alcohol was from Merck Millipore, India, and used as such without any further purification.

**2.2. Synthesis of Sorbent.** 3-Aminopropyl triethoxysilane (AS, 30.4579 g) and vinyl triethoxysilane (VS, 26.2090 g) were mixed in absolute ethanol/water mixture so that the molar concentration of silane/ethanol/water in the mixture is 1:30:8. The mixture was stirred for 3 h and aged in a closed vessel at ambient temperature for 5 days. After aging, the system was diluted by adding 5 L of ethanol, shaken well, sprayed on to glass plates using a spray gun, and kept under sunlight. The material that formed was vacuum-dried at 85 °C for 1 h. Yield: 17.2 g. The material was designated as MAHSM (monoamine-based hybrid silica material).

2.3. Characterization. Elemental analysis was performed using PerkinElmer 2400 CHNS analyzer with a thermal conductivity detector. The morphology of the sample was obtained through field emission scanning electron microscopy (FE-SEM, JEOL Microscope JSM 6060). Microstructure of the sample was evaluated using transmission electron microscope model FEI (Tecnai G2 30 S-TWIN) with an accelerating voltage of 300 kV. For TEM measurements, the sample dispersed in acetone was drop-casted on the carbon-coated copper grid and dried in vacuum at room temperature before observation. Infrared spectra of the samples were recorded using PerkinElmer Spectrum GX A FTIR spectrometer in the wavelength region 4000-400 cm<sup>-1</sup> with a spectral resolution of 4 cm<sup>-1</sup> by making a pellet with dry KBr. Solid-state <sup>13</sup>C and <sup>29</sup>Si NMR experiments were performed using a Bruker AVANCE 400 spectrometer (9.4 T), operating at Larmor frequencies of 100.6 and 79.5 MHz, respectively, equipped with a Bruker cross-polarization magic angle spinning (CP-MAS) probe and 4 mm  $ZrO_2$  rotors, spinning at 5 kHz. For <sup>13</sup>C, the <sup>1</sup>H-<sup>13</sup>C CP-MAS pulse sequence was employed with optimized contact time of 2 ms and a repetition time (D1) of 5 s. <sup>29</sup>Si MAS NMR spectra were acquired by using  $^{1}H-^{29}Si$ cross-polarization (CP-MAS) with contact time of 5 ms. Adamantane was used as the external references for <sup>13</sup>C (methine resonance at 38.5

ppm) and peak of tetrakis(trimethylsilyl)silane (TTMS) at -9.8 ppm for  $^{29}$ Si NMR measurements.

XRD measurements were carried out by a Bruker D8-Discover Xray diffractometer operating with a Cu anode (40 kV, 40 mA) keeping the sample on a zero background Si sample cup. Diffractograms were recorded using Lynx Eye solid-state detector from 5° to 50° at a step size 0.02° and time/step 0.5 s. TG-MS analysis was done using PerkinElmer Pyris 1 TGA coupled with Clarus SQ8T quadruple mass spectrometer through a heated fused silica transfer line. The transfer line temperature was maintained at 210 °C, and the evolved species were ionized in electron impact ionization mode with electron energy of 70 eV. Mass spectra of the evolved species were recorded for a mass range 10-500 amu. Thermogravimetric analyses were done with PerkinElmer Pyris 1 thermogravimetric analyzer in inert atmosphere (helium), with heating rate of 10 °C/min. The heat of absorption of CO<sub>2</sub> was obtained from differential scanning calorimetry (DSC) technique using TA Instrument DSC Q20 maintaining isothermal conditions and measuring heat flow to or from the sample cell. The absorption was performed in a flow of pure CO<sub>2</sub> (100 mL/min) at 30 °C. The heat of adsorption was calculated by integrating heat flow over the time period of adsorption. Raman imaging was performed using Witec Alpha 300R confocal Raman microscope equipped with 100× air objective and 600 grooves/mm grating. Surface scan of  $(14 \times 18)$  $\mu$ m<sup>2</sup> and depth scan (5  $\mu$ m) were done using 532 nm laser source and a back illuminated CCD detector. Surface area was determined using Quanta chrome Nova 1200e surface area analyzer using the Brunauer-Emmett-Teller (BET) method. The material was heated at 150 °C under helium flow for 15 min before any characterization technique.

**2.4. CO**<sub>2</sub> **Adsorption/Desorption Studies.** Thermogravimetric Method. CO<sub>2</sub> adsorption/desorption studies were carried out using a PerkinElmer Pyris 1 thermogravimetric analyzer with purge gas switching accessory with about 10 mg of sample in a platinum pan. Pure CO<sub>2</sub> (99.99%), CO<sub>2</sub>–N<sub>2</sub> mixture (10:90), and ambient air (400 ppm at RH 60%) were used for CO<sub>2</sub> adsorption studies. The CO<sub>2</sub> adsorption capacity was estimated from the weight gain of the sorbent after exposure to CO<sub>2</sub> using a gas flow rate of 100 mL/min. Desorption studies were done at 80 °C under He flow (70 mL/min). The material was heated at 150 °C under He flow (30 mL/min) for 15 min before any CO<sub>2</sub> adsorption study.

The cyclic regeneration studies of the sorbent materials were also done with TG analyzer using 100%  $CO_2$  and ambient air under the same conditions used in adsorption/desorption as detailed above.

Packed Column Adsorption. MAHSM (12.0 g) was packed in a glass tube (20 cm  $\times$  3 cm). The material was heated at 150 °C under N<sub>2</sub> flow (100 mL/min) for 15 min. After cooling, ambient air (RH 85%, 28 °C) containing 350 ppm of CO<sub>2</sub> was passed through the sorbent at a flow rate of 500 mL/min. The input and output CO<sub>2</sub> concentrations were measured using IR detector.

#### 3. RESULTS AND DISCUSSION

**3.1. Synthesis of Sorbent and Characterization.** The sorbent was developed on the basis of the hydrolytic cocondensation reaction of amino propyl and vinyl functionalized triethoxysilanes.<sup>51</sup> Aminosilane acts as internal catalyst for the hydrolysis and condensation reactions in the silane mixture. Different types of silsesquioxanes, viz., cage, ladder, and network, were reported to be formed by hydrolytic cocondensation reactions.<sup>50–54</sup> A general scheme for the reaction is shown in Scheme S1. The optimizations of the mole ratio of silanes/ethanol/water, stirring time, aging period, and final molar concentration of silanes/ethanol/water for the preparation of hybrid silica materials were done on the basis of the  $CO_2$  adsorption/desorption performance and thermal stability of the product material. Aminosilane (AS) and vinylsilane (VS) at 1:1 molar ratio was optimized for an aging period of 5 days (Tables S1 and S2).

In the synthesis of the material, after aging the silane mixture it was diluted with absolute alcohol before spraying down to make the final product (MAHSM). The morphology of the material changed as revealed from the SEM images as shown in Figure 1. The "bottleneck" regions as visible in Figure 1a were

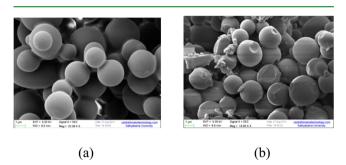


Figure 1. Change in morphology of MAHSM (a) material as such prepared from aged siloxane solution and (b) material prepared after dilution of aged siloxane solution.

broken, and discrete microspheres  $(1-3.5 \ \mu\text{m})$  were formed as in Figure 1b when prepared after dilution of aged siloxane solution. An interesting feature observed was that CO<sub>2</sub> capture capacity increased when the material was prepared after dilution (Table S1). This can be explained as possibly due to the more "exposed reaction sites" (amino groups) made available for CO<sub>2</sub> by breaking the agglomeration and forming independent microspheres upon dilution.

FT-IR spectrum (Figure S1) of MAHSM features Si–O–Si<sub>str</sub> at 1138 and 1039 cm<sup>-1</sup>. The peak 1138 cm<sup>-1</sup> is characteristic of caged (T<sub>8</sub>) silsesquioxane, <sup>55–57</sup> and the one at 1039 cm<sup>-1</sup> may be attributed to ladder/network polysilsesquioxane. <sup>57–59</sup> Also, the "peak shape" in 1030–1130 cm<sup>-1</sup> range is generally being considered as the characteristic of structured silsesquioxane. <sup>60</sup> Other spectral bands are for vinyl (3060, 1410 cm<sup>-1</sup>), amino propyl (3367, 3291, 2933, and 1602 cm<sup>-1</sup>), and Si–OH (964 cm<sup>-1</sup>).

Solid-state <sup>13</sup>C and <sup>29</sup>Si CP-MAS NMR data (Figure S2) were used to characterize the chemical structure of the material. <sup>13</sup>C CP-MAS NMR spectra showed resonance peaks at 131.9 and 135.2 ppm corresponding to vinyl groups. Peaks at 11.3, 25.2, and 44.4 ppm represent the  $-(CH_2)_3NH_2$  moiety. <sup>29</sup>Si CP-MAS NMR spectra showed peaks at -80.1 and -66.8 ppm corresponding to fully condensed T<sup>3</sup> vinyl and amino propyl species, respectively. A small shoulder peak at -57.6 ppm is due to T<sup>2</sup> species resulting from incomplete condensation. NMR

data suggest relatively fully condensed polysilsesquioxane formation in MAHSM.

Raman spectrum (Figure S3) showed a peak at 483 cm<sup>-1</sup> corresponding to Si-O-Sistr (sym) of cross-linked network siloxane.<sup>61</sup> Other peaks of interest are 1600 cm<sup>-1</sup> ( $-NH_2$  sci),  $3303 \text{ cm}^{-1}$  (-NH<sub>2</sub> sym),  $3370 \text{ cm}^{-1}$  (-NH<sub>2</sub> asym), and 1408 $cm^{-1}$  (vinyl). A Raman spectral image as in Figure 2a was generated by scanning over an area of  $(14 \times 18) \, \mu m^2$  MAHSM aggregate and integrating over characteristic amine and vinyl vibrations, and the Raman spectra remained the same throughout the area of scan. In the image, the black portion corresponds to substrate on which the sample is placed, and the red/yellow part corresponds to the sample. It can be seen that the Raman image is similar to the SEM image of MAHSM, showing hybrid silica microspheres. The line scan (x-y scan)and depth scan (z) using the wavelengths 1600 cm<sup>-1</sup> ( $-NH_2$ ) sci), 3303 cm<sup>-1</sup> (-NH<sub>2</sub> sym), and 1408 cm<sup>-1</sup> (vinyl) generated the same cross-sectional profile as in Figure 2b indicating vinyl and amine moieties are homogeneously distributed throughout the material.

The wave-like pattern in the cross-sectional profile (through the blue line in the image) is due to the spherical nature of the particle which causes a change in focus during scan, and the distances between consecutive troughs give the diameter of the sphere-like particles.

The C/N ratio of MAHSM was calculated from elemental analysis (C 26.1%, H 4.8%, N 6.3%). Eight different batches of MAHSM were analyzed, and these studies found that the C/N mole ratio falls at 4.9  $\pm$  0.3 which is close to the theoretical value (5.0). This further confirms the homogeneity of sorbent with respect to amine and vinyl distribution as inferred from Raman imaging. Low BET surface area (0.9 m<sup>2</sup>/g) and SEM analysis point out that hybrid silica sorbent synthesized through this method is not mesoporous.

The XRD pattern shows broad reflections at  $2\theta$  values of 8.8° and 22° (Figure S4). Generally, peaks at ~8° and ~20° are regarded as characteristic crystalline reflections from caged silsesquioxanes, and in particular, the peak at 8° is attributed to the *d*-spacing caused by the size of the polyhedral oligomeric silsesquioxane (POSS) molecule. Pavithran et al.<sup>51</sup> assigned the peak at 8° to POSS and the one at 20° to hexagonal or rhombohedral packing of POSS cages in siloxane polymeric halo. In the case of MAHSM, the XRD pattern obtained was of diffused type conforming more toward amorphous nature. The  $2\theta$  and *d* values (8.8°, 10.1 Å) are close to the values reported

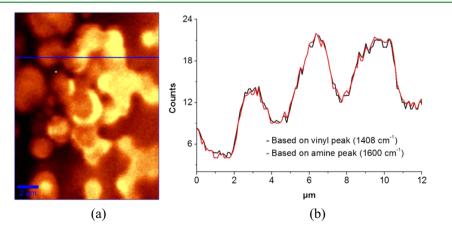


Figure 2. (a) Raman image and (b) cross-sectional profile across the line in part a.

for POSS-polymer nanocomposites.<sup>62-64</sup> A similar XRD pattern and *d* values were reported for ladder or network polysilsesquioxane also.<sup>53,54</sup>

Even though the IR spectrum and XRD pattern of hybrid silica indicate the formation of POSS cage, the IR peak at 1030 cm<sup>-1</sup> corresponds to the formation of ladder/network silsesquioxane, and Raman peak at 483 cm<sup>-1</sup> indicates crosslinked network silsesquioxane. The hybrid silica material is insoluble in all common organic solvents, suggesting the formation of cross-linked network silsesquioxanes. Thus, the possibility of the existence of cage, ladder, and network silsesquioxane together in the material cannot be ruled out. As the existence of ladder silsesquioxanes in our system is not proven unambiguously, on the basis of the available information, the hybrid silica materials are better viewed as crystalline aggregates of POSS cages distributed in cross-linked network silsesquioxane polymer. Lei Zheng et al. proposed an ordered arrangement of cubic silsesquioxane nanoparticles in the polyethylene-*co*-POSS<sup>62</sup> system and, later, for the polybutadiene-POSS nanocomposite system.<sup>64</sup> In the present case, the self-aggregation of POSS nanoparticles can happen in network silsesquioxane polymer and will be controlled by vinyl and amino groups. The hydrophobic vinyl groups help in deciding the orientation of amino groups and lead to a "relatively structured" polysilsesquioxane hybrid silica material. The layered structure of MAHSM is evident in the HR-TEM image (Figure 3).

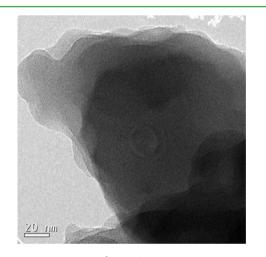


Figure 3. HR-TEM image of MAHSM.

The thermal stability of MAHSM is confirmed by thermogravimetric analysis (Figure S5) which shows that the sorbents are stable up to 300 °C under inert atmosphere. The organic matter decomposes above 300 °C resulting in the formation of stable residue at 800 °C. The decomposition temperature for 5% weight loss,  $T_{d}$  (5%), obtained for MAHSM was 458 °C which shows the quality of the material for using it as a thermally regenerable sorbent.

**3.2.** CO<sub>2</sub> Adsorption Characteristics. The hybrid silica sorbent, MAHSM, was analyzed for CO<sub>2</sub> adsorption capacity using thermogravimetric analyzer under different partial pressures of CO<sub>2</sub>. MAHSM showed a maximum CO<sub>2</sub> adsorption of 2.28 mmol/g in 100% CO<sub>2</sub> and 1.92 mmol/g in 10% CO<sub>2</sub>, at a flow rate of 100 mL/min at 30 °C. The experimental adsorption capacity of MAHSM in 100% CO<sub>2</sub> is closely matching with the theoretical value of 2.25 mmol/g

(assuming 100% carbamate conversion for an amine content of 4.5 mmol N/g of MAHSM). The heat of absorption value of  $-85 \pm 5$  kJ/mol CO<sub>2</sub> obtained from isothermal differential scanning calorimetry (Figure S6) for 3 different measurements indicates that the process involving adsorption of CO<sub>2</sub> to MAHSM is a chemical interaction.

The sorbent was also evaluated for the adsorption of  $CO_2$ from ambient air (containing 400 ppm of  $CO_2$ , 60% RH) at 30 °C with a flow rate of 100 mL/min in 24 h, and a  $CO_2$ adsorption capacity of 1.68 mmol/g was obtained. A comparison of  $CO_2$  adsorption by MAHSM under different  $CO_2$  partial pressures is shown in Figure 4.

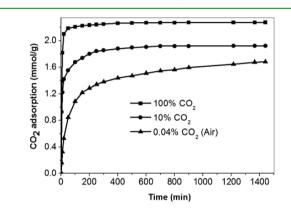


Figure 4. Comparison of  $CO_2$  adsorption of MAHSM at different  $CO_2$  concentration.

The CO<sub>2</sub> adsorption studies using 100% CO<sub>2</sub>, 10% CO<sub>2</sub>, and air (0.04% CO<sub>2</sub>) suggest that the adsorption capacity of the hybrid silica sorbent is not depreciated significantly even with ultradilution in CO<sub>2</sub> concentration. When the CO<sub>2</sub> concentration was reduced by a factor of 250 (from 10% to 400 ppm), the adsorption capacity of MAHSM decreased only by a factor of 1.1 showing the capability of the sorbent to capture CO<sub>2</sub> from extreme dilutions. It may be noted that for HAS sorbents this factor was reported as 2.2.<sup>44</sup> The TG-MS analysis of the sorbent material after CO<sub>2</sub> adsorption from ambient air (Figure S7) shows a peak corresponding to CO<sub>2</sub> (*m*/*z* 44) alone. Thus, it is confirmed that the total weight gain after adsorption from air is entirely due to CO<sub>2</sub>. Absence of a moisture peak in TG-MS points toward the hydrophobic nature of the sorbent.

Further, it was observed that CO<sub>2</sub> adsorption from ambient air decreases with increase of temperature (Figure S8). The CO<sub>2</sub> adsorption capacity decreased from 1.68 mmol/g at 30 °C to 1.08 mmol/g at 50 °C. The adsorption half time (time for reaching half of the adsorption capacity at saturation) and average rate of adsorption to reach the half-maximum were used for comparison among reported sorbents by many researchers. Choi et al.<sup>36,44</sup> compared the adsorption half time  $(T_{half})$ , and Gebald et al.<sup>65</sup> additionally used average rate of  $CO_2$  adsorption to reach  $T_{half}$  for comparison among different adsorbents. MAHSM showed an adsorption half time of 50 min reached at the rate of 17.9  $\mu$ mols/g/min during CO<sub>2</sub> capture from air under the given conditions of the experiment. An amine efficiency (37.3%) of MAHSM  $(1.68 \text{ mmol CO}_2 \text{ from air})$ by 4.5 mmol N) in air capture is far better than many of the reported materials. Table S3 shows a comparison among similar regenerable sorbents reported for direct CO<sub>2</sub> capture from ambient air.

Lab level studies were conducted to evaluate the  $CO_2$  adsorption behavior from ambient air (RH 85%, 28 °C containing 350 ppm of  $CO_2$ ), with higher sample loading, using a separate packed column setup. Figure 5 shows the result obtained for  $CO_2$  adsorption from air using a packed column experiment.

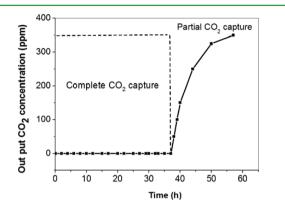


Figure 5. Adsorption of CO<sub>2</sub> from air using packed column.

The first part represents the complete adsorption of  $CO_2$ from air giving zero output  $CO_2$  concentration, which lasted for 37 h. After this period, the material started to get saturated slowly and gave output  $CO_2$  concentration ranging from 50 to 200 ppm, which continued until 56 h, and got fully saturated. The total  $CO_2$  adsorption from ambient air was 19.1 mmol of  $CO_2$  by 12.0 g of sorbent corresponding to 1.59 mmol  $CO_2/g$ . Desorption was done at 80 °C under N<sub>2</sub> flow (100 mL/min) for 30 min. This experiment, given the worst environment for capturing  $CO_2$  competing with moisture and other gases in air, proves the efficiency of MAHSM as a real  $CO_2$  capturing material.

The quick adsorption of  $CO_2$  from extreme dilution as that from atmospheric air is attributed to the easy accessibility of primary amino groups, a direct output from the layered arrangement of polysilsesquioxanes. The layered structure further helps in the easy regeneration of  $CO_2$ . Also, hydrophobic nature of the material kept away moisture when compared to sorbent systems based on mesoporous materials.

**3.3.** CO<sub>2</sub> Desorption Characteristics. Desorption starts at a lower temperature, 60 °C, and >50% desorption is completed within 5 min, but complete desorption happens at 80 °C in 10 min (Figure S9). Figure S10 shows the IR spectra of MAHSM after CO<sub>2</sub> adsorption (a) and desorption (b). The peaks at 1642 (NH<sub>3</sub><sup>+</sup> def), 1568 (asym COO<sup>-</sup>), 1489 (sym NH<sub>3</sub><sup>+</sup> def),

and 1340 cm<sup>-1</sup> (sym COO<sup>-</sup>) are indicative of CO<sub>2</sub> adsorption/ desorption.<sup>66-68</sup> It may be noted that all these peaks are corresponding to the weak ionic carbamate species formed with the amino groups, and there are no bound carbamates as evidenced by the absence of peaks at 1710–1715 cm<sup>-1</sup> (C=O str) and 1510 cm<sup>-1</sup> (NH def + C–N str). The bound carbamate moiety (1715–1710 cm<sup>-1</sup>) was assigned as silyl propyl carbamate (Figure S11) by Zoltan Bacsik et al.<sup>68</sup> in agreement with the findings of Danon et al.<sup>66</sup>

Even though silanol groups are present, the hydrophobic vinyl groups decide the orientation of the POSS aggregation and minimize silanol–carbamic acid interaction, thereby preventing silyl propyl carbamate formation. This again emphasizes the stable orientation of POSS and network silsesquioxane in the sorbent system as discussed. The absence of bound carbamate (silyl propyl carbamate) in the present sorbent is beneficial in the easy regeneration after  $CO_2$  adsorption and will ultimately be helpful in giving high cyclic utility and life for the sorbent.

**3.4. Cyclic Studies.** In 100%  $CO_2$ , adsorption is very fast, and >80% of the reaction is completed in less than 15 min. Hence, the adsorption/desorption half cycles were fixed at 15 min. Up to 100 cycles of regeneration (Figure 6) were successfully demonstrated using MAHSM without any loss in efficiency.

The cyclic ability of MAHSM for the removal of  $CO_2$  from ambient air (400 ppm of  $CO_2$ , 30 °C, RH 60%) was also demonstrated. As  $CO_2$  adsorption capacity of MAHSM reaches >1.0 mmol/g in 100 min, adsorption was performed for 100 min, and desorption was done for 15 min. Figure 7 shows 50 consecutive regeneration cycles performed in ambient air with MAHSM.

Urea formation is reported as a side reaction that could limit the cyclic utility of amine sorbents. Sayari et al.<sup>69</sup> studied the CO2 induced degradation of grafted amine sorbents and reported that, after 30 thermal cycles at 50/130 °C of monoamine-based sorbent, the carbamate carbonyl peak (<sup>13</sup>C CP-MAS NMR) at 164.5 ppm shifted to 159.6 ppm suggesting the formation of urea which resulted in 65% CO<sub>2</sub> uptake loss. In the case of MAHSM, 50 cycles were performed at 30 °C in ambient air followed by desorption at 80 °C under He flow. The sorbent, after the 1st and 50th adsorption cycles, was analyzed by <sup>13</sup>C CP-MAS NMR, and the peak appeared at 164.5 ppm in both cases. To check whether the lack of urea formation is due to residual moisture resulting from low regeneration temperature, 40 regeneration cycles of adsorption at 30 °C (100% CO<sub>2</sub> 100 mL/min, 15 min) and desorption at 120 °C (He flow, 70 mL/min, 15 min) were done. As in the

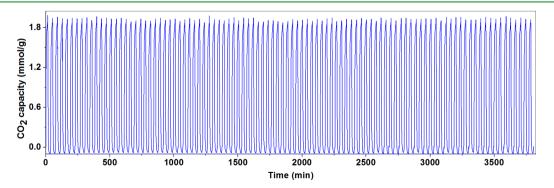


Figure 6. Cyclic capacity of MAHSM (100 cycles) in pure CO<sub>2</sub>.

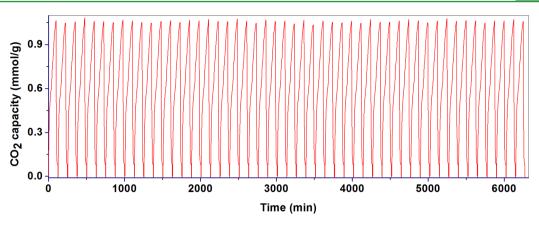


Figure 7. Cyclic capacity of MAHSM (50 cycles) in ambient air.

case of cycling from air, no shift in carbamate peak position (Figure S12) or loss in  $CO_2$  adsorption efficiency was observed.

#### 4. CONCLUSIONS

Functionalized polysilsesquioxane-based structured hybrid silica materials are developed as regenerable sorbents for the removal of carbon dioxide from atmospheric air. The developed material (MAHSM) captured a maximum of 1.68 mmol/g CO<sub>2</sub> from ambient air in 24 h, with an adsorption half time of 50 min reached at the rate of 17.9  $\mu$ mols/g/min, indicating a suitable candidate for air capture applications. CO2 adsorption capacities of 2.28 mmol/g in pure CO<sub>2</sub> and 1.92 mmol/g in 10% CO<sub>2</sub> were also demonstrated. Easy and energy efficient production route, low temperature regeneration, and high CO<sub>2</sub> cyclic capability make these materials "interesting" candidates for the CO<sub>2</sub> removal process. This material can also find application in closed habitats like submarines, space craft crew cabins, or any other systems requiring CO<sub>2</sub>-free air. Apart from the inherent CO<sub>2</sub> selectivity provided by the amino groups, the hydrophobic nature of the material prevents moisture uptake from air and hence can be further explored as hydrophobic coating materials capturing CO<sub>2</sub> directly from the atmosphere.

#### ASSOCIATED CONTENT

#### **S** Supporting Information

Scheme S1, Figures S1–S12, and Tables S1–S3. The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acsami.5b04674.

(PDF)

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#### Notes

The authors declare no competing financial interest.

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## ABBREVIATIONS

AS = 3-amino propyl triethoxysilane

VS = vinyl triethoxysilane

MAHSM = monoamine-based hybrid silica material

TRI-PE-MCM-41 = triamine-grafted pore expanded mesoporous silica

HAS = hyperbranched amino silica

POSS = polyhedral oligomeric silsesquioxane

AEAPDMS-NFC-FD = aminosilane modified nanofibrillated cellulose aerogel

MOF = metal organic framework

CP-MAS = cross-polarization-magic angle spinning

NMR = nuclear magnetic resonance spectroscopy

FTIR = Fourier transform infrared spectroscopy

FESEM = field emission scanning electron microscopy

HRTEM = high resolution transmission electron microscopy

TGA = thermogravimetric analyzer

GC-MS = gas chromatography-mass spectrometry

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